

## LISTING OF CLAIMS

1. (Original) A process for producing a dilute ethylene stream and a dilute propylene stream from a cracked gas stream, said process comprising the following steps in the order named:
  - (1) separating said cracked gas stream in a deethanizer zone to produce a  $C_2$  – stream and a  $C_3+$  stream;
  - (2). hydrogenating said  $C_2$ - stream in a hydrogenation zone to remove a portion of the acetylene to produce said dilute ethylene stream;
  - (3) separating said  $C_3+$  stream in a depropanizer zone to produce a  $C_3$ - stream and a  $C_4+$  stream; and
  - (4) reacting said  $C_3$ - stream in a MAPD reactor zone to convert a portion of methylacetylene and propadiene to propylene and propane to produce said dilute propylene stream.
2. (Original) A process according to claim 1 further comprising separating said  $C_4+$  stream in a debutanizer zone to produce a  $C_4$  stream and a  $C_5+$  stream.
3. (Original) A process according to claim 1 further comprising passing said dilute ethylene stream to a dilute ethylene derivative unit.
4. (Previously presented) A process according to claim 1 wherein said dilute ethylene derivative unit produces ethylbenzene.
5. (Original) A process according to claim 1 further comprising passing said dilute propylene stream to a dilute propylene derivative unit.
6. (Original) A process according to claim 5 wherein said dilute propylene derivative unit produces cumene, acrylic acid or propylene oxide.
7. (Original) A process according to claim 2 further comprising treating said  $C_5+$  stream in a hydrotreating zone to produce a  $C_5$  diolefins stream, a BTX stream, a DCPD stream and a fuel oil stream.

8. (Original) A process according to claim 1 wherein said cracked gas stream is produced by a process comprising:

(1) heating a hydrocarbon feed in a cracking zone to form a raw cracked gas stream; wherein said raw cracked gas stream comprises hydrogen, methane, C<sub>2</sub> hydrocarbons, C<sub>3</sub> hydrocarbons and heavier constituents;

(2) quenching said raw cracked gas stream in a quenching zone to produce a quenched, cracked gas stream;

(3) compressing said quenched, cracked gas stream in a first compression zone to form a pressurized, cracked gas stream;

(4) deacidifying said pressurized, cracked gas stream in a deacidifying zone to remove a portion of the hydrogen sulfide to form a wet cracked gas stream; and

(5) drying said wet cracked gas stream in a drying zone to form a cracked gas stream.

9. (Original) A process according to claim 8 wherein said hydrocarbon feed is selected from the group consisting of ethane, propane, butanes, pentanes, naphtha, and mixtures thereof.

10. (Original) A process according to claim 8 wherein said hydrocarbon feed consists essentially of C<sub>5</sub> hydrocarbons.

11. (Original) A process for producing a dilute ethylene stream and a dilute propylene stream from a cracked gas stream, said process comprising the following steps in the order named:

(1) separating said cracked gas stream in a deethanizer zone to produce a C<sub>2</sub> – stream and a C<sub>3</sub>+ stream;

(2) compressing said C<sub>2</sub>- stream in a compression zone to form a pressurized C<sub>2</sub>- stream;

(3) hydrogenating said pressurized C<sub>2</sub>- stream in a hydrogenation zone to remove a portion of the acetylene to produce said dilute ethylene stream;

(4) separating said  $C_3+$  stream in a depropanizer zone to produce a  $C_3-$  stream and a  $C_4+$  stream; and

(5) reacting said  $C_3-$  stream in a MAPD reactor zone to convert a portion of methylacetylene and propadiene to propylene and propane to produce said dilute propylene stream.

12. (Original) A process according to claim 11 further comprising separating said  $C_4+$  stream in a debutanizer zone to produce a  $C_4$  stream and a  $C_5+$  stream.

13. (Original) A process according to claim 11 further comprising passing said dilute ethylene stream to a dilute ethylene derivative unit.

14. (Original) A process according to claim 13 wherein said dilute ethylene derivative unit produces ethylbenzene.

15. (Original) A process according to claim 11 further comprising passing said dilute propylene stream to a dilute propylene derivative unit.

16. (Original) A process according to claim 15 wherein said dilute propylene derivative unit produces cumene, acrylic acid, or propylene oxide.

17. (Original) A process according to claim 12 further comprising treating  $C_5+$  stream in a hydrotreating zone to produce a  $C_5$  diolefins stream, a BTX stream, a DCPD stream, and a fuel oil stream.

18. (Original) A process according to claim 11 wherein said cracked gas stream is produced by a process comprising:

(1) heating a hydrocarbon feed in a cracking zone to form a raw cracked gas stream; wherein said raw cracked gas stream comprises hydrogen, methane,  $C_2$  hydrocarbons,  $C_3$  hydrocarbons, and heavier constituents;

(2) quenching said raw cracked gas stream in a quenching zone to produce a quenched, cracked gas stream;

(3) compressing said quenched, cracked gas stream in a first compression zone to form a pressurized cracked gas stream;

(4) deacidifying said pressurized, cracked gas stream in a deacidifying zone to remove a portion of the hydrogen sulfide to form a wet cracked gas stream; and

(5) drying said cracked gas stream in a drying zone to produce a cracked gas stream.

19. (Original) A process according to claim 18 wherein said hydrocarbon feed is selected from the group consisting of ethane, propane, butanes, pentanes, naphtha, and mixtures thereof.

20. (Original) A process according to claim 18 wherein said hydrocarbon feed consists essentially of C<sub>5</sub> hydrocarbons.

21. (Original) A process for producing a dilute ethylene stream and a dilute propylene stream from a cracked gas stream, said process comprising the following steps in the order named:

(1) hydrogenating a portion of the acetylene in said cracked gas stream in a hydrogenation zone to produce a reduced acetylene cracked gas stream;

(2) separating said reduced acetylene cracked gas stream in a deethanizer zone to produce said dilute ethylene stream and a C<sub>3</sub>+ stream;

(3) separating said C<sub>3</sub>+ stream in said depropanizer zone to produce a C<sub>3</sub>- stream and a C<sub>4</sub>+ stream; and

(4) reacting said C<sub>3</sub>- stream in a MAPD reactor zone to convert a portion of methylacetylene and propadiene to propylene and propane to produce the dilute propylene stream.

22. (Original) A process according to claim 21 further comprising separating said C<sub>4</sub>+ stream in a debutanizer zone to produce a C<sub>4</sub> stream and a C<sub>5</sub>+ stream.

23. (Original) A process according to claim 21 further comprising passing said dilute ethylene stream to a dilute ethylene derivative unit.

24. (Original) A process according to claim 21 wherein said dilute ethylene derivative unit produces ethylbenzene.
25. (Original) A process according to claim 21 further comprising passing said dilute propylene stream to a dilute propylene derivative unit.
26. (Original) A process according to claim 25 wherein said dilute propylene derivative unit produces cumene, acrylic acid, or propylene oxide.
27. (Original) A process according to claim 22 further comprising treating C<sub>5</sub>+ stream in a hydrotreating zone to produce a C<sub>5</sub> diolefins stream, a BTX stream, a DCPD stream, and a fuel oil stream.
28. (Original) A process according to claim 21 wherein said cracked gas stream is produced by a process comprising:
- (1) heating a hydrocarbon feed in a cracking zone to form a raw cracked gas stream; wherein said raw cracked gas stream comprises hydrogen, methane, C<sub>2</sub> hydrocarbons, C<sub>3</sub> hydrocarbons, and heavier constituents;
  - (2) quenching said raw cracked gas stream in a quenching zone to produce a quenched, cracked gas stream;
  - (3) compressing said quenched, cracked gas stream in a first compression zone to form a pressurized, cracked gas stream;
  - (4) deacidifying said pressurized, cracked gas stream in a deacidifying zone to remove a portion of the hydrogen sulfide to form a wet cracked gas stream; and
  - (5) drying said cracked stream in a drying zone to produce a cracked gas stream.
29. (Original) A process according to claim 25 wherein said hydrocarbon feed is selected from the group consisting of ethane, propane, butanes, pentanes, naphtha and mixtures thereof.

30. (Original) A process according to claim 25 wherein said hydrocarbon feed consists essentially of  $C_5$  hydrocarbons.

31. (Original) A process for producing a dilute ethylene stream and a dilute propylene stream, said process comprising the following steps in the order named:

(1) heating a hydrocarbon feed in a cracking zone to form a raw cracked gas stream; wherein said cracked gas stream comprises hydrogen, methane,  $C_2$  hydrocarbons,  $C_3$  hydrocarbons and heavier constituents;

(2) quenching said raw cracked gas stream in a quenching zone to produce a quenched, cracked gas stream;

(3) compressing said quenched, cracked gas stream in a first compression zone to form a pressurized cracked gas stream;

(4) deacidifying said pressurized, cracked gas stream in a deacidifying zone to remove a portion of the hydrogen sulfide to form a wet cracked gas stream;

(5) drying said wet cracked gas stream in a drying zone to produce a cracked gas stream.

(6) separating said cracked gas stream in a deethanizer zone to produce a  $C_2^-$  stream and a  $C_3^+$  stream;

(7) compressing said  $C_2^-$  stream in a second compression zone to form a pressurized  $C_2^-$  stream;

(8) hydrogenating said pressurized  $C_2^-$  stream in a hydrogenation zone to remove a portion of the acetylene to produce said dilute ethylene stream; and

(9) separating said  $C_3^+$  stream in a depropanizer zone to produce said dilute propylene stream and a  $C_4^+$  stream.

- (10) reacting said C<sub>3</sub>- stream in a MAPD reactor zone to convert a portion of methylacetylene and propadiene to propylene and propane to produce said dilute propylene stream.
32. (Original) A process according to claim 31 further comprising separating said C<sub>4</sub>+ stream in a debutanizer zone to produce a C<sub>4</sub> stream and a C<sub>5</sub>+ stream.
33. (Original) A process according to claim 32 further comprising treating C<sub>5</sub>+ stream in a hydrotreating zone to produce a C<sub>5</sub> diolefins stream, a BTX stream, a DCPD stream, and a fuel oil stream.
34. (Original) A process according to Claim 31 further comprising passing said dilute ethylene stream to a dilute ethylene derivative unit.
35. (Original) A process according to claim 34 wherein said dilute ethylene derivative unit produces ethylbenzene.
36. (Original) A process according to claim 31 further comprising passing said dilute propylene stream to a dilute propylene derivative unit.
37. (Original) A process according to claim 36 wherein said dilute propylene derivative unit produces cumene, acrylic acid or propylene oxide.
38. (Original) A process according to claim 31 wherein said hydrocarbon feed is selected from the group consisting of ethane, propane, butanes, pentanes, naphtha and mixtures thereof.
39. (Original) A process according to claim 31 wherein said hydrocarbon feed consists essentially of C<sub>5</sub> hydrocarbons.
40. (Original) A process for producing a dilute ethylene stream and a dilute propylene stream, said process comprising the following steps in the order named:

(1) heating a hydrocarbon feed in a cracking zone to form a cracked gas stream; wherein said cracked gas stream comprises hydrogen, methane, C<sub>2</sub> hydrocarbons, C<sub>3</sub> hydrocarbons, and heavier constituents;

(2) quenching said raw cracked gas stream in a quenching zone to produce a quenched, cracked gas stream;

(3) compressing said quenched, cracked gas stream in a first compression zone to form a pressurized cracked gas stream;

(4) deacidifying said pressurized, cracked gas stream in a deacidifying zone to remove a portion of the hydrogen sulfide to form a wet cracked gas stream;

(5) drying said wet cracked gas stream in a drying zone to produce a cracked gas stream;

(6) separating said cracked gas stream in a deethanizer zone to produce a C<sub>2</sub>- stream and a C<sub>3</sub>+ stream;

(7) hydrogenating said pressurized, C<sub>2</sub>- stream in said hydrogenation zone to remove a portion of the acetylene to produce said dilute ethylene stream; and

(8) separating said C<sub>3</sub>+ stream in a depropanizer zone to produce said dilute propylene stream and a C<sub>4</sub>+ stream.

(9) reacting said C<sub>3</sub>- stream in a MAPD zone to convert a portion of methylacetylene and propadiene to propylene and propane to produce said dilute propylene stream.

41. (Original) A process according to claim 40 further comprising separating said C<sub>4</sub>+ stream in a debutanizer zone to produce a C<sub>4</sub> stream and a C<sub>5</sub>+ stream.

42. (Original) A process according to claim 40 further comprising treating C<sub>5</sub>+ stream in a hydrotreating zone to produce a C<sub>5</sub> diolefins stream, a BTX stream, a DCPD stream, and a fuel oil stream.



43. (Original) A process according to Claim 40 further comprising passing said dilute ethylene stream to a dilute ethylene derivative unit.
44. (Original) A process according to Claim 43 wherein said dilute ethylene derivative unit produces ethylbenzene.
45. (Original) A process according to Claim 40 further comprising passing said dilute propylene stream to a dilute propylene derivative unit.
46. (Original) A process according to Claim 45 wherein said dilute propylene derivative unit produces cumene, acrylic acid, or propylene oxide.
47. (Original) A process according to claim 40 wherein said hydrocarbon feed is selected from the group consisting of ethane, propane, ethane-propane mix, butanes, pentanes and naphtha and mixtures thereof.
48. (Original) A process according to claim 40 wherein said hydrocarbon feed consists essentially of C<sub>5</sub> hydrocarbons.
49. (Original) A process for producing a dilute ethylene stream and a dilute propylene stream from a cracked gas stream, said process comprising the following steps in the order named:
- (1) heating a hydrocarbon feed in a cracking zone to form a raw cracked gas stream; wherein said raw cracked gas stream comprises hydrogen, methane, C<sub>2</sub> hydrocarbons, C<sub>3</sub> hydrocarbons, and heavier constituents;
  - (2) quenching said raw cracked gas stream in a quenching zone to produce a quenched, cracked gas stream;
  - (3) compressing said quenched, cracked gas stream in a first compression zone to form a pressurized cracked gas stream;
  - (4) deacidifying said pressurized, cracked gas stream in a deacidifying zone to remove a portion of the hydrogen sulfide to form a wet cracked gas stream; and

- (5) drying said cracked gas stream in a drying zone to produce a cracked gas stream.
  - (6) hydrogenating a portion of the acetylene in said cracked gas stream in a hydrogenation zone to produce a reduced acetylene cracked gas stream;
  - (7) separating said reduced acetylene cracked gas stream in a deethanizer zone to produce said dilute ethylene stream and a C<sub>3</sub>+ stream;
  - (8) separating said C<sub>3</sub>+ stream in said depropanizer zone to produce a C<sub>3</sub>- stream and a C<sub>4</sub>+ stream; and
  - (9) reacting said C<sub>3</sub>- stream in a MAPD reactor zone to convert a portion of methylacetylene and propadiene to propylene and propane to produce the dilute propylene stream.
50. (Original) A process according to claim 49 further comprising separating said C<sub>4</sub>+ stream in a debutanizer zone to produce a C<sub>4</sub> stream and a C<sub>5</sub>+ stream.
51. (Original) A process according to claim 49 further comprising passing said dilute ethylene stream to a dilute ethylene derivative unit.
52. (Original) A process according to claim 51 wherein said dilute ethylene derivative unit produces ethylbenzene.
53. (Original) A process according to claim 49 further comprising passing said dilute propylene stream to a dilute propylene derivative unit.
54. (Original) A process according to claim 53 wherein said dilute propylene derivative unit produces cumene, propylene oxide, or acrylic acid.
55. (Original) A process according to claim 50 further comprising treating C<sub>5</sub>+ stream in a hydrotreating zone to produce a C<sub>5</sub> diolefins stream, a BTX stream, a DCPD stream, and a fuel oil stream.

56. (Original) A process according to claim 49 wherein said hydrocarbon feed is selected from the group consisting of ethane, propane, butanes, pentanes, naphtha and mixtures thereof.
57. (Original) A process according to claim 49 wherein said hydrocarbon feed consists essentially of  $C_5$  hydrocarbons.
58. (Original) A process for producing a dilute ethylene stream and a dilute propylene stream from a cracked gas stream, said process comprising the following steps in the order named:
- (1) separating said cracked gas stream in a deethanizer zone to produce a  $C_2$  – stream and a  $C_3+$  stream;
  - (2). hydrogenating said  $C_2$ - stream in a hydrogenation zone to remove a portion of the acetylene to produce said dilute ethylene stream;
  - (3) routing said  $C_3+$  stream to storage or other process unit.
59. (Original) A process according to claim 58 further comprising passing said dilute ethylene stream to a dilute ethylene derivative unit.
60. (Original) A process according to claim 59 wherein said dilute ethylene derivative unit produces ethylbenzene.
61. (Original) A process for producing a dilute ethylene stream from a cracked gas stream, said process comprising the following steps in the order named:
- (1) separating said cracked gas stream in a deethanizer zone to produce a  $C_2$  – stream and a  $C_3+$  stream;
  - (2) compressing said  $C_2$ - stream in a compression zone to form a pressurized  $C_2$ - stream;
  - (3) hydrogenating said pressurized  $C_2$ - stream in a hydrogenation zone to remove a portion of the acetylene to produce said dilute ethylene stream;
  - (4) routing said  $C_3+$  stream to storage or other process unit.

62. (Original) A process according to claim 61 further comprising passing said dilute ethylene stream to a dilute ethylene derivative unit.

63. (Original) A process according to claim 62 wherein said dilute ethylene derivative unit produces ethylbenzene.

64. (Original) A process for producing a dilute ethylene stream from a cracked gas stream, said process comprising the following steps in the order named:

(1) hydrogenating a portion of the acetylene in said cracked gas stream in a hydrogenation zone to produce a reduced acetylene cracked gas stream;

(2) separating said reduced acetylene cracked gas stream in a deethanizer zone to produce said dilute ethylene stream and a C<sub>3</sub>+ stream;

(3) routing said C<sub>3</sub>+ stream to storage or other process unit.

65. (Original) A process according to claim 64 further comprising passing said dilute ethylene stream to a dilute ethylene derivative unit.

66. (Original) A process according to claim 65 wherein said dilute ethylene derivative unit produces ethylbenzene.

67. (Original) A process for producing a dilute ethylene stream said process comprising the following steps in the order named:

(1) heating a hydrocarbon feed in a cracking zone to form a raw cracked gas stream; wherein said cracked gas stream comprises hydrogen, methane, C<sub>2</sub> hydrocarbons, C<sub>3</sub> hydrocarbons and heavier constituents;

(2) quenching said raw cracked gas stream in a quenching zone to produce a quenched, cracked gas stream;

(3) compressing said quenched, cracked gas stream in a first compression zone to form a pressurized cracked gas stream;

(4) deacidifying said pressurized, cracked gas stream in a deacidifying zone to remove a portion of the hydrogen sulfide to form a wet cracked gas stream;

(5) drying said wet cracked gas stream in a drying zone to produce a cracked gas stream.

(6) separating said cracked gas stream in a deethanizer zone to produce a C<sub>2</sub>- stream and a C<sub>3</sub>+ stream;

(7) compressing said C<sub>2</sub>- stream in a second compression zone to form a pressurized C<sub>2</sub>- stream;

(8) hydrogenating said pressurized C<sub>2</sub>- stream in a hydrogenation zone to remove a portion of the acetylene to produce said dilute ethylene stream; and

(9) routing said C<sub>3</sub>+ stream to storage or other process unit.

68. (Original) A process according to claim 67 further comprising passing said dilute ethylene stream to a dilute ethylene derivative unit.

69. (Original) A process according to claim 68 wherein said dilute ethylene derivative unit produces ethylbenzene.

70. (Original) A process for producing a dilute ethylene stream, said process comprising the following steps in the order named:

(1) heating a hydrocarbon feed in a cracking zone to form a cracked gas stream; wherein said cracked gas stream comprises hydrogen, methane, C<sub>2</sub> hydrocarbons, C<sub>3</sub> hydrocarbons, and heavier constituents;

(2) quenching said raw cracked gas stream in a quenching zone to produce a quenched, cracked gas stream;

(3) compressing said quenched, cracked gas stream in a first compression zone to form a pressurized cracked gas stream;

(4) deacidifying said pressurized, cracked gas stream in a deacidifying zone to remove a portion of the hydrogen sulfide to form a wet cracked gas stream;

(5) drying said wet cracked gas stream in a drying zone to produce a cracked gas stream;

(6) separating said cracked gas stream in a deethanizer zone to produce a C<sub>2</sub>- stream and a C<sub>3</sub>+ stream;

(7) hydrogenating said pressurized, C<sub>2</sub>- stream in said hydrogenation zone to remove a portion of the acetylene to produce said dilute ethylene stream; and

(8) routing said C<sub>3</sub>+ stream to storage or other process unit.

71. (Original) A process according to claim 70 further comprising passing said dilute ethylene stream to a dilute ethylene derivative unit.

72. (Original) A process according to claim 70 wherein said dilute ethylene derivative unit produces ethylbenzene.

73. (Original) A process for producing a dilute ethylene stream, said process comprising the following steps in the order named:

(1) heating a hydrocarbon feed in a cracking zone to form a raw cracked gas stream; wherein said raw cracked gas stream comprises hydrogen, methane, C<sub>2</sub> hydrocarbons, C<sub>3</sub> hydrocarbons, and heavier constituents;

(2) quenching said raw cracked gas stream in a quenching zone to produce a quenched, cracked gas stream;

(3) compressing said quenched, cracked gas stream in a first compression zone to form a pressurized cracked gas stream;

(4) deacidifying said pressurized, cracked gas stream in a deacidifying zone to remove a portion of the hydrogen sulfide to form a wet cracked gas stream; and

- (5) drying said cracked gas stream in a drying zone to produce a cracked gas stream.
  - (6) hydrogenating a portion of the acetylene in said cracked gas stream in a hydrogenation zone to produce a reduced acetylene cracked gas stream;
  - (7) separating said reduced acetylene cracked gas stream in a deethanizer zone to produce said dilute ethylene stream and a C<sub>3</sub>+ stream;
  - (8) routing said C<sub>3</sub>+ stream to storage or other process unit.
74. (Original) A process according to claim 73 further comprising passing said dilute ethylene stream to a dilute ethylene derivative unit.
75. (Original) A process according to claim 73 wherein said dilute ethylene derivative unit produces ethylbenzene.